

I claim:

1. A process for purifying a naphthalenic carboxylic acid comprising contacting an impure naphthalenic acid and a purification solvent in the presence of hydrogen with a catalyst comprising a Group VIII noble metal at a purification temperature of from about 520 to 575 °F.

2. The process of Claim 1 wherein the naphthalenic carboxylic acid is 2,6-naphthalenedicarboxylic acid.

3. The process of Claim 1 wherein the noble metal is palladium.

4. The process of Claim 1 wherein the noble metal is deposited on a carbon support.

5. The process of Claim 1 wherein the acid is 2,6-naphthalenedicarboxylic acid prepared by the liquid phase, heavy metal catalyzed oxidation of 2,6-dimethylnaphthalene.

6. The process of Claim 1 wherein the noble metal is palladium on a carbon support, and wherein the naphthalenic carboxylic acid is 2,6-naphthalenedicarboxylic acid.

7. The process of Claim 6 wherein the 2,6-naphthalenedicarboxylic acid for purification is prepared by the liquid phase, heavy metal catalyzed oxidation of 2,6-dimethylnaphthalene.

8. The process of Claim 1 wherein the purification temperature is about 525°F to about 560°F.

9. The process of Claim 1 wherein the total percent dissolved solids in the purification solvent is less than twelve weight percent, based on the total weight of solids plus solvent.

10. The process of Claim 7 wherein the total percent dissolved solids in the purification solvent is less than ten weight percent, based on the total weight of solids plus solvent, and wherein the purification temperature is about 525°F to about 560°F.

11. The process of Claim 1 which is performed in a purification reactor designed to operate at a nominal operating temperature no greater than about 550°F.

12. The process of Claim 6 which is performed in a purification reactor designed to operate at a nominal operating temperature no greater than about 550°F.

13. The process of Claim 10 which is performed in a purification reactor

designed to operate at a nominal operating temperature no greater than about 550°F.

14. The process of Claim 1 wherein the purified acid is recovered by solid liquid separation at a temperature of between about 300 and 340 °F.

15. The process of Claim 6 wherein the purified acid is recovered by solid liquid separation at a temperature of between about 300 and 340 °F.

16. The process of Claim 10 wherein the purified acid is recovered by solid liquid separation at a temperature of between about 300 and 340 °F.

17. The process of Claim 1 wherein the catalyst further includes a Group IVB metal selected from the group consisting from silicon, germanium, tin or lead.

10 18. The process of Claim 17 wherein the Group IVB metal is tin.

19. The process of Claim 17 wherein the Group IVB metal is present at between 0.2 to 0.6 weight percent of the total catalyst weight.

20. The process of Claim 18 wherein the tin is present at between 0.2 to 0.6 weight percent of the total catalyst weight and the noble metal is ruthenium, which is present at between 0.1 to 3.0 weight percent total catalyst weight.